

JAYPEE UNIVERSITY OF INFORMATION TECHNOLOGY, WAKNAGHAT
TEST -3 EXAMINATION- Dec 2017
B.Tech (BT) IIIrd Semester

MAX. MARKS:35

COURSE CODE: 10B11BT311

COURSE NAME: Thermodynamics and Chemical processes

COURSE CREDITS: 4

MAX. TIME: Two Hours

Note: All questions are compulsory. Carrying of mobile phone during examinations will be treated as case of unfair means.

- Q1(a). How the lineweaver-burk plot and Langmuir plot are useful for the calculations of Michaelis-Menten constants? 3
- (b). 1 mole of an ideal gas, ($C_v = 12.471 \text{ JK}^{-1} \text{ mol}^{-1}$) is heated from 300 K to 600K. Calculate entropy change when (i) volume is kept constant and (ii) pressure is kept constant. ($R = 8.314 \text{ JK}^{-1} \text{ mol}^{-1}$) 3
- Q2. Consider the following interconversion, which occurs in glycolysis :
Fructose-6-phosphate \leftrightarrow glucose-6-phosphate ($K'_{eq} = 1.97$)
- (a) What is ΔG° for the reaction (assuming that the temperature is 25°C)? 3
- (b) If the concentration of fructose-6-phosphate is adjusted to 1.5 M and that of glucose-6-phosphate is adjusted to 0.5 M, what is ΔG ? 3
- Q3(a). Elucidate the flow system for energy balance equations. 3
- (b). Classification of non newtonian fluids depends upon the relationship between shear stress and shear strain. Justify this statement by giving equations and graphs. 4
- Q4(a). Discuss how viscosity is calculated in an impeller viscometer. 2
- (b). Draw the proper flow sheet and mass balance table for the following material balances:
Acetobacter aceti bacteria convert ethanol to acetic acid under aerobic conditions as shown below. A continuous fermentation process for vinegar production is proposed using non-viable *A. aceti* cells immobilised on the surface of gelatin beads. The production target is 2 Kg h^{-1} acetic acid, however the maximum acetic acid concentration tolerated by the cells is 12 %. Air is pumped into the fermenter at a rate of 200 gmol h^{-1} 4
- Q5. From the following data:
- | Shear stress (dyn cm^{-2}) | Shear rate (s^{-1}) |
|---------------------------------------|--------------------------------|
| 44.1 | 10.2 |
| 235.3 | 170 |
| 357.1 | 340 |
| 457.1 | 510 |
| 636.8 | 1020 |
- (a) Plot the rheogram for this fluid.
- (b) Determine the appropriate non-Newtonian parameters. 5
- (c) What is the apparent viscosity at shear rates of 15 s^{-1}
- Q6(a). In double-tube pass heat exchanger, flow of tube and shell fluids is mainly countercurrent for one tube pass and mainly cocurrent for the other. Justify this statement. 4
- (b). How the overall heat-transfer coefficient can be expressed in terms of individual resistances to heat transfer? 4