

COURSE CODE: 18B11BT511

MAX. MARKS: 35

COURSE NAME: Bioprocess Engineering

COURSE CREDITS: 04

MAX. TIME: 2 Hours

*Note: All questions are compulsory. Carrying of mobile phone during examinations will be treated as case of unfair means. For calculations, you may use simple/scientific calculator.*

1. a) Determine the doubling time of a bacterial culture if it has specific growth rate  $0.6 \text{ hr}^{-1}$ .  
[CO3] [1]  
b) Why the chemostat in series is better than using a single chemostat fermenter for the production of recombinant products?  
[CO3] [2]
2. If a medium and the product formed generates more foam, so how will you deal with such conditions while running a fermenter?  
[CO2] [2]
3. Determine the dead band value of pH in a fermenter system if you wish to run it at set value of 7.0. Here the dead band should lie in the range of 8% of the set value. [CO5] [2]
4. For an aerobic culture which bioreactor will you use: Fermenter A which has  $K_L a$  value =  $0.2 \text{ sec}^{-1}$  or Fermenter B having  $K_L a$  value =  $0.4 \text{ sec}^{-1}$ ? Give a proper justification of your selection.  
[CO2, CO4] [2]
5. An industrial fermentor containing 10,000 L of medium needs to be sterilized. The initial spore concentration in the medium is  $10^6$  spores  $\text{mL}^{-1}$ . The desired probability of contamination after sterilization is  $10^{-3}$ . The death rate of spores at  $121^\circ \text{C}$  is  $4 \text{ min}^{-1}$ . Assume that there is no cell death during heating and cooling phases. Determine the holding time of the sterilization process in min.  
[CO3, CO4] [2]
6. List the 3 independent and 3 dependent variables with their units. [CO1] [3]

7. Which bioreactor is more efficient in mass and heat transfer from the following: Justify your answer with the appropriate reasons and diagram. [CO5] [4]
- Airlift bioreactor and bubble column
  - Fixed Bed Bioreactor and Fluidized bed Bioreactor
8. Differentiate between (At least 3 main differences) [CO1, CO5] [6]
- Static and Dynamic Gassing out method
  - Airlift bioreactor with internal loop and with external loop
9. A genetically-engineered strain of bacteria is cultured in a bioreactor at 35°C for production of a heterologous protein. The oxygen requirement is 80 mmol l<sup>-1</sup>h<sup>-1</sup>; the critical oxygen concentration is 0.004 mM. The solubility of oxygen in the fermentation broth is estimated to be 10% lower than in water due to solute effects. The solubility of oxygen in pure water at 1 atm pressure is 8.05 x 10<sup>-3</sup> Kg m<sup>-3</sup>. Calculate the minimum mass-transfer coefficient required to sustain this culture if the reactor is sparged with air at approximately 1 atm pressure? [CO4] [4]
10. a) If the height-to-diameter ratio remains constant, then what happened to the surface-to-volume ratio during scaling up? How will it affect the bioprocess during scaling up? [2]
- b) A stirred-tank reactor is to be scaled down from 10 m<sup>3</sup> to 0.1 m<sup>3</sup>. The dimensions of the large tank are:  $D_t = 2$  m;  $D_i = 0.5$  m;  $N = 100$  rpm. Determine the dimensions of the small tank ( $D_t$ ,  $D_i$ ,  $H$ ) by using geometric similarity. [CO6] [3]
- c) For the above question, what would be the required rotational speed of the impeller in the small tank if we use Constant tip speed as the scale down criteria? [CO6] [2]