

COURSE CODE: 15B11BT511

MAX. MARKS: 25

COURSE NAME: BIOPROCESS ENGINEERING

COURSE CREDITS: 04

MAX. TIME: 1.5 Hr.

Note: All questions are compulsory. Carrying of mobile phone during examinations will be treated as case of unfair means.

[CO I, V]

1. i) Why is it important to run fermenter at positive pressure? [1]
- ii) How does the Kolmogorov scale link with the shear forces generation in the agitated fermenter? [2]
- ii) How does the foam control system work? [2]
2. Write down the functions of following components of the fermenter: [4]
- a) Baffles
- b) Head Space Volume
- c) Load Cell
- d) Sparger
3. Differentiate between following: [3]
- a) Axial flow Impeller and Radial flow Impeller
- b) Dynamic and static Gassing out Method

[CO II]

4. i) Cells become metabolically disturbed if DO level drops below C_{crit} . In some cases, metabolic disturbance due to this may be advantageous. Whether this statement is correct? Justify your answer with suitable at least two examples. [2]
- ii) If you wish to improve the volumetric mass transfer coefficient ($k_L a$) value of a fermenter, what factors will you consider while designing and operating a fermentation process? [2]

[CO III, IV]

5. A fermentation broth with viscosity 10^{-2} Pa s and density 1000 kg m^{-3} is agitated in a 2.7 m^3 baffled tank using a Rushton turbine with diameter 0.5 m and stirrer speed 1 s^{-1} . Estimate the mixing time. [2]
6. i) Determine the time (in minutes) required to reduce the number of viable spores from an initial value of 10^{10} to a final value of 1 if k_d value is 1.0 min^{-1} . [2]
- ii) Sterilization at higher temperatures for shorter periods of time has the advantage of killing cells with limited destruction of medium components. Whether this statement is correct? Justify your answer. [2]

7. Ethanol is to be used as a substrate for single-cell protein production in a chemostat. The available equipment can achieve an oxygen transfer rate of 10 g O₂/l of liquid per hour. Assume the kinetics of cell growth on ethanol is of the Monod type, with $\mu_{\max} = 0.5 \text{ h}^{-1}$, $K_S = 30 \text{ mg/l}$, $Y_{X/S} = 0.5 \text{ cells/g ethanol}$, and $Y_{O_2/S} = 2 \text{ g O}_2/\text{g EtOH}$. We wish to operate the chemostat with an ethanol concentration in the feed of 22 g/L. We also wish to maximize the biomass productivity and minimize the loss of unused ethanol in the effluent. Determine the required dilution rate and whether sufficient oxygen can be provided. [3]

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